

The Lecture Contains:

 [2.5 Approximate Methods for Flat Plate Boundary Layer](#)

 [Previous](#) [Next](#) 

2.5 Approximate Methods for Flat Plate Boundary Layer

Flow over a heated flat plate $\left[Pr \sim \frac{\delta}{\delta_T} \text{ from } \frac{\delta}{\delta_T} \sim (Pr)^{1/3} \text{ or } \frac{\delta}{\delta_T} \sim (Pr)^{1/2} \right]$ has been illustrated.

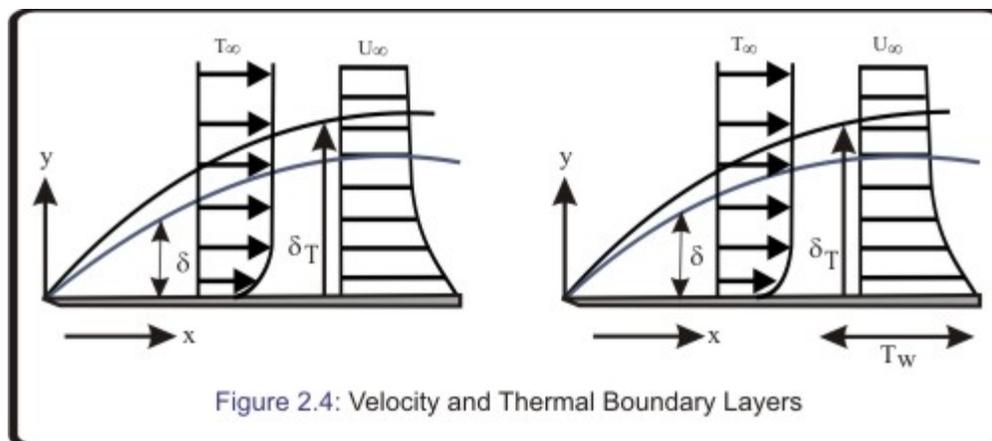


Figure 2.4: Velocity and Thermal Boundary Layers

Governing Equations :

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \quad (2.85)$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial v}{\partial y} = -\frac{1}{\rho} \frac{dp}{dx} + \nu \frac{\partial^2 u}{\partial y^2} \quad (2.86)$$

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \frac{k}{\rho c_p} \frac{\partial^2 T}{\partial y^2} \quad (2.87)$$

The boundary conditions are :

$$\text{@ } y = 0, u = 0 = v, T = T_w$$

$$\text{@ } y = \delta, u = U_\infty, \text{ @ } y = \delta_T, T = T_\infty$$

Using Integral method due to **von Karman and Pohlhausen** is written as eqn. (2.86)

$$\underbrace{\int_0^\delta u \frac{\partial u}{\partial x} dy}_{\text{I}} + \underbrace{\int_0^\delta v \frac{\partial u}{\partial y} dy}_{\text{II}} = \underbrace{\int_0^\delta -\frac{1}{\rho} \frac{dp}{dx} dy}_{\text{III}} + \underbrace{\int_0^\delta \nu \frac{\partial^2 u}{\partial y^2} dy}_{\text{IV}}$$

Term III is zero for flow over flat plate (because $dp/dx = 0$)

II term:

$$[vu]_0^\delta - \int_0^\delta \frac{\partial v}{\partial y} u dy = [vu|_\delta - vu|_0] + \int_0^\delta u \frac{\partial u}{\partial x} dy \quad (\text{from continuity}) \quad (2.88)$$

Module 2: External Flows

Lecture 9: Approximate Solutions of Boundary Layer Equations

Again, from continuity :

$$\frac{\partial u}{\partial x} = -\frac{\partial v}{\partial y}$$

or ,

$$\int_0^\delta \frac{\partial v}{\partial y} dy = -\int_0^\delta \frac{\partial u}{\partial x} dy$$

or ,

$$v|_{y=\delta} = -\int_0^\delta \frac{\partial u}{\partial x} dy$$

II term finally becomes :

$$-U_\infty \int_0^\delta \frac{\partial u}{\partial x} dy + \int_0^\delta u \frac{\partial u}{\partial x} dy$$

Equation (2.88) can be written as :

$$2 \int_0^\delta u \frac{\partial u}{\partial x} dy - U_\infty \int_0^\delta \frac{\partial u}{\partial x} dy = -\nu \frac{\partial u}{\partial y} \Big|_{y=0}$$

or ,

$$\frac{d}{dx} \int_0^\delta u^2 dy - U_\infty \frac{d}{dx} \int_0^\delta u dy = -\nu \frac{\partial u}{\partial y} \Big|_{y=0} \quad (2.89)$$

Equation (2.89) is **Momentum Integral Equation**. Let us assume :

$$u = C_0 + C_1 y + C_2 y^2 + C_3 y^3$$

$$\frac{u}{U_\infty} = C_0 + C_1 \eta + C_2 \eta^2 + C_3 \eta^3, \quad \text{where } \eta = y/\delta$$

η is called similarity parameter; despite the growth of buoyancy layer in x direction $\frac{u}{U_\infty}$ remains similar for same $\frac{y}{\delta}$ at any x .

Boundary conditions:

$$\textcircled{a} y = 0, u = 0, \quad \text{or, } \textcircled{a} \eta = 0, \frac{u}{U_\infty} = 0, \quad \Rightarrow C_0 = 0$$

$$\textcircled{a} y = \delta, u = U_\infty, \quad \text{or, } \textcircled{a} \eta = 1, \frac{u}{U_\infty} = 1$$

$$\text{or, } [C_1 \eta + C_3 \eta^3]_{\eta=1} = 1, \quad \text{or, } C_1 + C_3 = 1$$

$$\textcircled{a} y = 0, \frac{\partial^2 u}{\partial y^2} = 0 \quad \left(\text{comes from } u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = \nu \frac{\partial^2 u}{\partial y^2} \right),$$

$$\text{or, } \textcircled{a} \eta = 0, \frac{\partial^2 (u/U_\infty)}{\partial \eta^2} = 0,$$

$$\text{or, } [2C_2 + 6C_3 \eta]_{\text{at } \eta=0} = 0 \Rightarrow C_2 = 0$$

$$\textcircled{a} y = \delta, \frac{\partial u}{\partial y} = 0 \quad \text{or, } \textcircled{a} \eta = 1, \frac{\partial}{\partial \eta} \left[\frac{u}{U_\infty} \right] = 0$$

$$\text{or, } [C_1 + 3C_3 \eta^2]_{\eta=1} = 0, \quad \Rightarrow C_1 + 3C_3 = 0$$

Finally we get,

$$C_1 = \frac{3}{2}, C_3 = -\frac{1}{2} \quad \text{So, } \frac{u}{U_\infty} = \frac{3}{2} \eta - \frac{1}{2} \eta^3$$

Integral of the first term in **equation (2.89)**

$$\int_0^\delta u^2 dy = \frac{U_\infty^2}{4} \int_0^1 [9\eta^2 + \eta^6 - 6\eta^4] \delta d\eta$$

$$= \frac{\delta U_\infty^2}{4} \left[\frac{9}{3} + \frac{1}{7} - \frac{6}{5} \right] = \frac{68}{35} \frac{\delta U_\infty^2}{4}$$

Module 2: External Flows

Lecture 9: Approximate Solutions of Boundary Layer Equations

Integral associated with the second term of **equation (2.89)**

$$\int_0^\delta u dy = \frac{U_\infty}{2} \int_0^1 [3\eta - \eta^3] \delta d\eta = \frac{5 U_\infty \delta}{4}$$

The third term of **equation (2.89)** $-\nu \frac{\partial u}{\partial y} \Big|_{y=0}$

$$\begin{aligned} &= -\frac{\nu}{\delta} \frac{\partial}{\partial \eta} \left[U_\infty \left(\frac{3}{2}\eta - \frac{1}{2}\eta^3 \right) \right] \Big|_{\eta=0} \\ &= -\frac{3\nu U_\infty}{2\delta} \end{aligned}$$

Finally **equation (2.89)** becomes :

$$\frac{U_\infty^2}{4} \frac{d\delta}{dx} \left[\frac{68}{35} - \frac{5}{2} \right] = -\frac{3 U_\infty \nu}{2\delta}$$

which reduces to

$$\delta \frac{d\delta}{dx} = \frac{140}{13} \frac{\nu}{U_\infty}$$

On integration this gives

$$\frac{1}{2} \frac{13}{140} \delta^2 = \frac{\nu x}{U_\infty} + C \quad (2.90)$$

Initial condition @ $x = 0, \delta = 0$ gives $C = 0$

Finally :

$$\delta = 4.64 \sqrt{\frac{\nu x}{U_\infty}}$$

On substituting $Re_x = \frac{U_\infty x}{\nu}$ we get,

$$\delta = 4.64 \frac{x}{\sqrt{Re_x}} \quad (2.91)$$

Module 2: External Flows

Lecture 9: Approximate Solutions of Boundary Layer Equations

Casting the integral form of thermal boundary layer equation :

$$\int_0^{\delta_T} u \frac{\partial T}{\partial x} dy + \int_0^{\delta_T} v \frac{\partial T}{\partial y} dy = \int_0^{\delta_T} \frac{k}{\rho c_p} \frac{\partial^2 T}{\partial y^2} dy \quad (2.92)$$

Integrating the second term by parts and applying continuity, we get :

$$\int_0^{\delta_T} u \frac{\partial T}{\partial x} dy + [vT]_0^{\delta_T} - \int_0^{\delta_T} T \frac{\partial v}{\partial y} dy = \left[\frac{k}{\rho c_p} \frac{\partial T}{\partial y} \right]_0^{\delta_T}$$

or $\int_0^{\delta_T} u \frac{\partial T}{\partial x} dy + \int_0^{\delta_T} T \frac{\partial u}{\partial x} dy + T_\infty v|_{\delta_T} = -\frac{k}{\rho c_p} \frac{\partial T}{\partial y} \Big|_{y=0}$

where $v|_{\delta_T} = -\int_0^{\delta_T} \frac{\partial u}{\partial x} dy$

or

$$\int_0^{\delta_T} \left(u \frac{\partial T}{\partial x} + T \frac{\partial u}{\partial x} \right) dy - T_\infty \int_0^{\delta_T} \frac{\partial u}{\partial x} dy = -\frac{k}{\rho c_p} \frac{\partial T}{\partial y} \Big|_{y=0}$$

or,

$$\int_0^{\delta_T} \frac{\partial}{\partial x} [u(T - T_\infty)] dy = -\frac{k}{\rho c_p} \frac{\partial T}{\partial y} \Big|_{y=0}$$

or ,

$$\frac{d}{dx} \int_0^{\delta_T} [u(T - T_\infty)] dy = -\frac{k}{\rho c_p} \frac{\partial T}{\partial y} \Big|_{y=0} \quad (2.93)$$

This **equation is called Energy Integral Equation**. In order to solve this, let us assume the temperature profile $\theta = \frac{T-T_w}{T_\infty-T_w} = C_0 + C_1\zeta + C_2\zeta^2 + C_3\zeta^3$. Where $\zeta = \frac{y}{\delta_T}$ is a similarity parameter.

Applying thermal boundary conditions:

$$\textcircled{a} \ y = 0; T = T_w, \Rightarrow \text{ at } \zeta = 0, \theta = 0 : C_0 = 0$$

$$\textcircled{a} \ y = 0; \frac{\partial^2 T}{\partial y^2} = 0, \Rightarrow \text{ at } \zeta = 0, \frac{d^2 \theta}{d\eta^2} = 0 : C_2 = 0$$

$$\textcircled{a} \ y = \delta_T; T = T_\infty, \Rightarrow \text{ at } \zeta = 1, \theta = 1 : C_1 + C_3 = 1$$

$$\textcircled{a} \ y = \delta_T; \frac{\partial T}{\partial y} = 0, \Rightarrow \text{ at } \zeta = 1, \frac{d\theta}{d\eta} = 0 : C_1 + 3C_3 = 0$$

Solving for C_1 and C_3 $C_1 = \frac{3}{2}$, and $C_3 = -\frac{1}{2}$. Therefore

$$\frac{T - T_w}{T_\infty - T_w} = \frac{3}{2}\zeta - \frac{1}{2}\zeta^3 \quad (2.94)$$

Now ,

$$\theta - 1 = \frac{T - T_w - T_\infty + T_w}{T_\infty - T_w} = \frac{T - T_\infty}{T_\infty - T_w}$$

or ,

$$(T - T_\infty) = (\theta - 1) (T_\infty - T_w)$$

First term of the energy integral (2.93) is:

$$(T_\infty - T_w) \frac{d}{dx} \int_0^{\delta_T} u(\theta - 1) dy$$

$$U_\infty (T_\infty - T_w) \frac{d}{dx} \int_0^{\delta_T} \left[\frac{3}{2}\eta - \frac{1}{2}\eta^3 \right] \left[\frac{3}{2}\zeta - \frac{1}{2}\zeta^3 - 1 \right] dy$$

$$U_\infty (T_\infty - T_w) \frac{d}{dx} \int_0^{\delta_T} \left[\frac{3}{2} \left(\frac{y}{\delta} \right) - \frac{1}{2} \left(\frac{y}{\delta} \right)^3 \right] \left[\frac{3}{2} \left(\frac{y}{\delta_T} \right) - \frac{1}{2} \left(\frac{y}{\delta_T} \right)^3 - 1 \right] dy$$

Substituting $\xi = \frac{\delta_T}{\delta}$ and rearranging, we get :

$$\begin{aligned} U_\infty (T_\infty - T_w) \frac{d}{dx} \left[\delta \left\{ \frac{3}{4}\xi^2 - \frac{3}{20}\xi^4 - \frac{3}{20}\xi^2 + \frac{1}{28}\xi^4 - \frac{3}{4}\xi^2 + \frac{1}{8}\xi^4 \right\} \right] \\ = U_\infty (T_\infty - T_w) \frac{d}{dx} \left[\delta \left\{ -\frac{3}{20}\xi^2 + \frac{3}{280}\xi^4 \right\} \right] \end{aligned}$$

The **RHS** of energy integral **equation (2.93)** is evaluated in the following way :

$$(T - T_w) = (T_\infty - T_w) \left[\frac{3}{2} \left(\frac{y}{\delta_T} \right) - \frac{1}{2} \left(\frac{y}{\delta_T} \right)^3 \right]$$

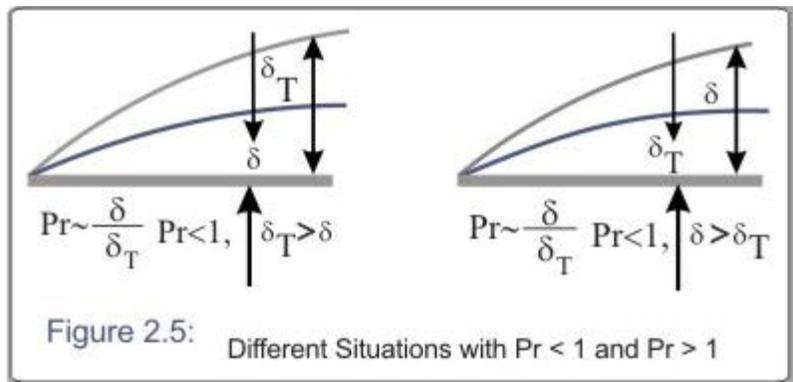
$$\frac{\partial T}{\partial y} = (T_\infty - T_w) \left[\frac{3}{2} \frac{1}{\delta_T} - \frac{3}{2} \frac{y^2}{\delta_T^3} \right]$$

$$-\frac{k}{\rho c_p} \frac{\partial T}{\partial y} \Big|_{y=0} = -\alpha \frac{3(T_\infty - T_w)}{2 \delta_T}$$

Now **equation (2.93)** becomes :

$$(T_\infty - T_w) U_\infty \frac{d}{dx} \left[\delta \left\{ -\frac{3}{20} \xi^2 + \frac{3}{280} \xi^4 \right\} \right] = -\frac{3\alpha(T_\infty - T_w)}{2 \delta_T} \quad (2.95)$$

For $Pr > 1$, $\delta > \delta_T$, $\xi = \frac{\delta_T}{\delta}$ becomes small, and so $\xi^4 \ll \xi^2$



For $Pr > 1$ (**Figure 2.5**), **equation (2.95)** becomes :

$$\delta U_\infty \frac{d}{dx} \left[\delta \frac{\xi^2}{20} \right] = \frac{\alpha}{2\xi}$$

$$\frac{10\alpha}{U_\infty \xi} = \delta \frac{d\delta}{dx} \xi^2 + \delta^2 \frac{d}{dx} \xi^2$$

where $\delta \frac{d\delta}{dx} = \frac{140 \nu}{13 U_\infty}$, and $\delta^2 = \frac{280 \nu x}{13 U_\infty}$

Finally, on substitution of the above two relations, **equation (2.95)** becomes :

$$\xi^3 + 2x\xi \frac{d}{dx}(\xi^2) = \frac{13}{14} \frac{1}{Pr} \quad (2.96)$$

◀◀ Previous Next ▶▶

Put $\chi = \xi^3$; $\frac{d\chi}{dx} = 3\xi^2 \frac{d\xi}{dx}$ substituting in **equation (2.96)**

$$\chi + \frac{4x}{3} \frac{d\chi}{dx} = \frac{13}{14} \frac{1}{Pr}$$

$$\frac{d\chi}{dx} + \frac{3}{4x} \chi = \frac{13}{14} \frac{1}{Pr} \frac{3}{4x}$$

This linear differential equation for which the integrating factor can be seen to be $x^{3/4}$

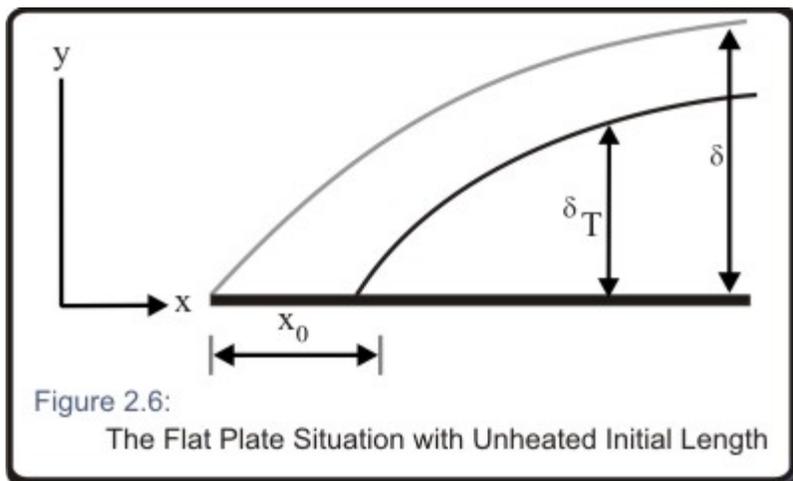
$$x^{3/4} \frac{d\chi}{dx} + \frac{3}{4} \frac{\chi}{x} x^{3/4} = \frac{13 \times 3}{14 \times 4} \frac{1}{Pr} x^{-1/4} \quad (2.97)$$

or

$$\frac{d}{dx} (x^{3/4} \chi) = \frac{39}{56} \frac{1}{Pr} x^{-1/4} \quad (2.98)$$

$$\chi = \frac{13}{14} \frac{1}{Pr} + b x^{-3/4} \quad (2.99)$$

where **b** is the constant of integration :



Module 2: External Flows

Lecture 9: Approximate Solutions of Boundary Layer Equations

Applying the boundary conditions as described in Figure 2.6, we get $x = x_0$, $\delta_T = 0$, $\xi = 0$; and so, $x = x_0$, $\chi = 0$. Substituting in **equation (2.99)**, we get :

$$b = -\frac{13}{14} \frac{1}{Pr} x_0^{3/4} \quad (2.100)$$

After substituting in **equation (2.99) for b**, we get :

$$\xi^3 = \chi = \frac{13}{14} \frac{1}{Pr} - \frac{13}{14} \frac{1}{Pr} \left(\frac{x_0}{x}\right)^{3/4}$$

For $x_0 \rightarrow 0$, we finally have :

$$\delta_T = \frac{\delta}{1.026} (Pr)^{-1/3} \quad (2.101)$$

Again we know that :

$$h(T_w - T_\infty) = -k \frac{\partial T}{\partial y} \Big|_{y=0}$$

On substituting for $\frac{\partial T}{\partial y} \Big|_{y=0}$ we get :

$$h = \frac{-k \frac{(T_\infty - T_w) \frac{3}{2}}{\delta_T}}{(T_w - T_\infty)}$$

Module 2: External Flows

Lecture 9: Approximate Solutions of Boundary Layer Equations

or,

$$h = k \frac{3}{2} \frac{1.026}{4.64x} (Pr)^{1/3} (Re_x)^{1/2}$$

(after invoking **equations (2.91) and (2.101)**)

The above expression leads to :

$$\frac{hx}{k} = 0.332(Re_x)^{1/2}(Pr)^{1/3}$$

The **local Nusselt number** can be expressed as:

$$Nu_x = 0.332(Re_x)^{1/2}(Pr)^{1/3} \quad (2.102)$$

Now, the average heat transfer coefficient $\bar{h} = \frac{\int_0^L h_x dx}{\int_0^L dx}$ and so the **average Nusselt number**

$$\overline{Nu_L} = \frac{\bar{h}L}{k} = 0.664(Re_L)^{1/2}(Pr)^{1/3} \quad (2.103)$$

Where, $Re_L = \frac{\rho U_\infty L}{\mu}$

◀ Previous Next ▶