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Mixed convection

The reference temperature be T_R and reference pressure P_R .

Thermal expansion number = $K_\rho = -\beta_R T_R$

Archimedes number = $\frac{K_\rho(1-T_w^*)}{F_R^2} = Ar$

Froude number = $\frac{V}{\sqrt{gl}} = F_R$

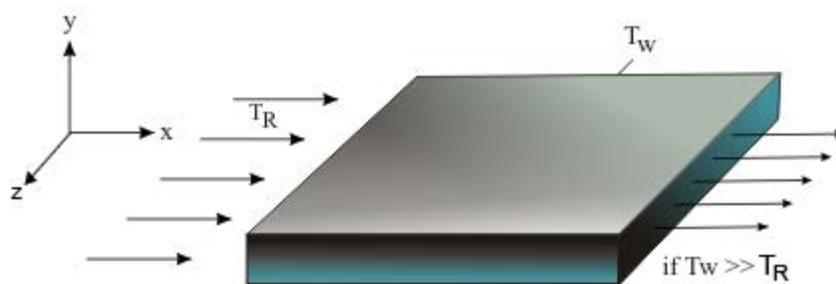


Figure 6.3: Buoyancy induced flow through horizontal channel

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$$Ar = \frac{\beta_R(T_w - T_R)gl}{V^2}$$

$$Gr = Ar * Re^2 = \frac{\beta_R(T_w - T_R)gl V^2 l^2}{V^2 \nu^2}$$

$$= \frac{\beta_R(T_w - T_R)gl^3}{\nu^2}$$

Figure 6.3 shows buoyancy induced flow through a horizontal channel.

The following are the governing equations

Continuity

$$\nabla \cdot u_i = 0$$

x momentum:

$$\frac{\partial u}{\partial t} + (\mathbf{V} \cdot \nabla)u = -\frac{1}{\rho} \frac{\partial p}{\partial x} + \nu \nabla^2 u$$

y momentum:

$$\frac{\partial v}{\partial t} + (\mathbf{V} \cdot \nabla)v = -\frac{1}{\rho} \frac{\partial p}{\partial y} + \nu \nabla^2 v + g\beta(T - T_\infty)$$

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z momentum:

$$\frac{\partial w}{\partial t} + (\mathbf{V} \cdot \nabla)w = -\frac{1}{\rho} \frac{\partial p}{\partial z} + \nu \nabla^2 w$$

Energy:

$$\frac{\partial T}{\partial t} + (\mathbf{V} \cdot \nabla)T = \alpha [\nabla^2 T]$$

After non-dimensionalization:

$$\begin{aligned} \nabla \cdot \mathbf{u}_i &= 0 \\ \frac{Du}{Dt} &= -\frac{\partial p}{\partial x} + \frac{1}{Re} \nabla^2 u \\ \frac{Dv}{Dt} &= -\frac{\partial p}{\partial y} + \frac{1}{Re} \nabla^2 v + \frac{Gr}{Re^2} \theta \end{aligned}$$

$$\frac{Dw}{Dt} = -\frac{\partial p}{\partial z} + \frac{1}{Re} \nabla^2 w$$

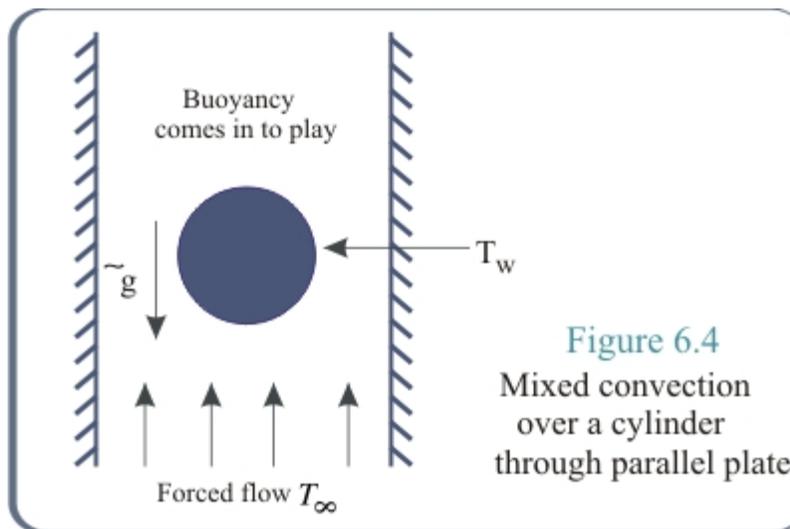
$$\frac{D\theta}{Dt} = \frac{1}{Re \cdot Pr} \nabla^2 \theta$$

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Depending on the problem (**heating/ cooling**), Ri can be positive and negative. Consider the following problem



$$T_w > T_\infty, Ri + ve$$

$$T_w < T_\infty, Ri - ve$$

In the mixed convection problem shown in **Figure 6.4** vortex shedding is found to stop completely at a critical Richardson number. The forced flow Reynolds number is 100. Explain why?

The following reference may be used

S.Singh, G.Biswas and A.Mukhopadhyay, Effect of Thermal Buoyancy on the Flow through a Vertical Channel with a Built-in Circular Cylinder, Numerical Heat Transfer, **Part-A, Vol. 34, pp. 769-789, 1998.**

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6.5.1 Exercise:

Start with a control volume approach (**Figure 6.5**) and find out an expression for the modified y -momentum equation for a mixed convection flow

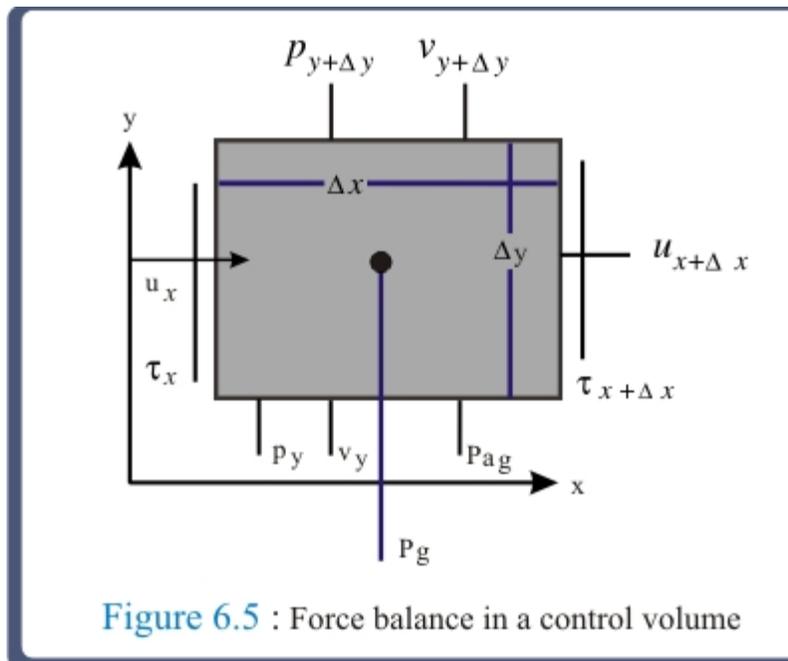
Newton's Second Law

Figure 6.5 : Force balance in a control volume

$$\sum F_y = (y \text{ - momentum outflux}) - (y \text{ - momentum influx})$$

Influx of y momentum through bottom face $(\rho v_y \Delta x) v_y$

Outflux of y momentum through top face $(\rho v_{y+\Delta y} \Delta x) v_{y+\Delta y}$

Influx of y momentum through left face $(\rho u_x \Delta y) v_x$

Outflux of y momentum through right face $(\rho u_{x+\Delta x} \Delta y) v_{x+\Delta x}$

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So,

$$\begin{aligned}
 p_y \Delta x - p_{y+\Delta y} \Delta x + \tau_{x+\Delta x} \Delta y - \tau_x \Delta y + \rho_\infty g \Delta x \Delta y - \rho g \Delta x \Delta y \\
 = \rho [(v v)_{y+\Delta y} \Delta x + (u v)_{x+\Delta x} \Delta y] \\
 - \rho [(v v)_y \Delta x + (u v)_x \Delta y]
 \end{aligned}$$

or

$$\begin{aligned}
 p_y \Delta x - \left(p_y + \frac{\partial p_y}{\partial y} \Delta y \right) \Delta x + \left(\tau_x + \frac{\partial \tau_x}{\partial x} \Delta x \right) \Delta y - \tau_x \Delta y + \rho_\infty g \Delta x \Delta y - \rho g \Delta x \Delta y \\
 = \rho \left[\left\{ (v v)_y + \frac{\partial (v v)_y}{\partial y} \Delta y \right\} \Delta x + \left\{ (u v)_x + \frac{\partial (u v)_x}{\partial x} \Delta x \right\} \Delta y \right] - \rho [(v v)_y \Delta x + (u v)_x \Delta y]
 \end{aligned}$$

or

$$\begin{aligned}
 -\frac{\partial p}{\partial y} \Delta x \Delta y + \frac{\partial \tau_x}{\partial x} \Delta x \Delta y + \rho_\infty g \Delta x \Delta y - \rho g \Delta x \Delta y \\
 = \rho \Delta x \Delta y \left[\frac{\partial}{\partial y} (v v)_y + \frac{\partial}{\partial x} (u v)_x \right]
 \end{aligned}$$

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$$\text{or,} \\ -\frac{\partial p}{\partial y} + \frac{\partial \tau_x}{\partial x} + \rho_\infty g - \rho g = \rho \left[v \frac{\partial v}{\partial y} + u \frac{\partial v}{\partial x} + v \left(\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} \right) \right]$$

$$\text{or,} \quad \rho \left(u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} \right) = -\frac{\partial p}{\partial y} + (\rho_\infty - \rho)g + \frac{\partial \tau_x}{\partial x}$$

References

B.Gebhart, Y. Jaluria , R . L . Mahajan and B Sammakia , **1988** , Buoyance Induced Flows.

Transport,Hemisphere Publishing Corporation Washington.

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