

## Module 2 : Convection

### Lecture 20 : Heat Transfer Enhancement Evaluation in Roughened Heat Exchanger Tubes

#### Objectives

##### In this class:

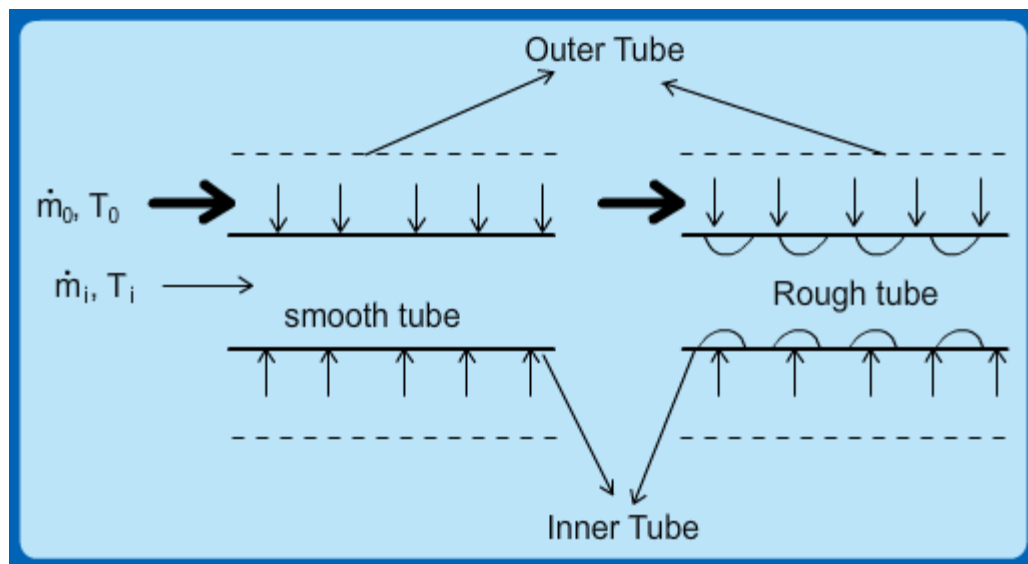
- Methodologies for evaluation of the performance of heat transfer enhancement devices in heat exchanger tubes of tube in tube type
- Material from "Application of Rough Surfaces to Heat Exchanger Design" R.L. Webb, R.L. & Eckert, E.R.G" International Journal of Heat and Mass Transfer pg. 1647, 1972

#### Rough Surface Heat Exchanger tubes-1

- The analysis in Class 19 was one where a heat flux was assumed to have been supplied to the pipe. Only the internal heat transfer coefficients were considered.
- Now consider a situation where outer wall of the tube is exposed to a fluid that transfers heat to the inner tube.
- Only the inner tube is assumed to have been roughened.

#### Rough Surface Heat Exchanger tubes-2

- There is now an outer heat transfer coefficient also.



#### Rough Surface Heat Exchanger tubes-3

- Let:
- $A_{os}, A_{or}, A_s, A_r$  = outer/inner surface of smooth/rough inner tube respectively.
- $h_o, h_s, h_r$  = heat transfer coefficients for outer tube, inner smooth/rough tube.
- Notice that even though  $A_s$  and  $A_r$  are not necessarily equal:

$$\frac{A_s}{A_{os}} = \frac{A_r}{A_{or}} = 1$$

#### Rough Surface Heat Exchanger tubes-4

- In this case the resistance to heat transfer due to the outer tube also needs to be considered and using a 1D analogy:

$$\frac{1}{UA} = \frac{1}{h_s A_s} + \frac{1}{h_o A_{os}} = \frac{1}{h_s A_s} \left[ 1 + \frac{h_s A_s}{h_o A_{os}} \right] \quad (20.1)$$

- U is the overall heat transfer coefficient. An equation like equ<sup>n</sup> (20.1) can also be written for the rough tube.
- Assume that the outer tube is not modified for enhancement and  $h_o$  remains constant

### Rough Surface Heat Exchanger tubes-5

- The smooth and rough heat exchangers need to be compared

$$\frac{1}{U_s A_s} = \frac{1}{h_s A_s} [1+r]; \quad (20.2)$$

$$\frac{1}{U_r A_r} = \frac{1}{h_r A_r} \left( 1 + r \frac{h_r}{h_s} \right) \quad (20.3)$$

$$r = \frac{h_s A_s}{h_0 A_{0s}} = \frac{h_s}{h_0}$$

- Now we can analyze in a manner similar to the previous situation.

### Rough Surface Heat Exchanger tubes-6

- Conductance ratio therefore becomes:

$$\frac{k_r}{k_s} = \frac{U_r A_r}{U_s A_s} = \frac{A_r}{A_s} \frac{(1+r)}{(h_s/h_r + r)} \quad (20.4)$$

- Heat transfer coefficient ratio for the inner smooth and rough situations is:

$$\frac{h_r}{h_s} = \frac{h_r \rho c_p u_r}{\rho c_p u_r} \frac{\rho c_p u_s}{h_s \rho c_p u_s} = \frac{St_r}{St_s} \frac{1}{g^*};$$

where  $\frac{\rho u_r}{\rho u_s} = \frac{1}{g^*}$  (20.5)

### Rough Surface Heat Exchanger tubes-7

- Therefore

$$\frac{k_r}{k_s} = \frac{A_r}{A_s} \left[ \frac{1+r}{g^* \frac{St_s}{St_r} + r} \right] \quad (20.6)$$

- Note that for  $r = 0$  equ<sup>n</sup>s (20.7) and (19.2) are identical; i.e. conductance in the previous case was infinite for the outer wall – this is alright since outer wall flux was specified i.e. resistance on outer wall is zero.
- Do the same manipulations as in the previous case and obtain the core equation.

### Rough Surface Heat Exchanger tubes-8

- The pumping power equation is the same as derived previously (i.e. equ<sup>n</sup> (19.8)):

$$\frac{P_r}{P_s} = \frac{f_r A_r}{f_s A_s} \left( \frac{1}{g^*} \right)^3 \quad (20.7)$$

- Substitute equ<sup>n</sup> (20.8) in equ<sup>n</sup> (20.7) to get:

$$\frac{k_r}{k_s} = \frac{A_r}{A_s} \left[ \frac{(1+r)}{\frac{(f_r/f_s)^{1/3} (A_r/A_s) St_s}{(P_r/P_s)^{1/3} St_r} + r} \right] \quad (20.8)$$

### Rough Surface Heat Exchanger tubes-9

- Equ<sup>n</sup> (20.9) is further simplified to yield

$$\begin{aligned} \frac{k_t}{k_s} \left( \frac{f_t}{f_s} \right)^{1/3} \left( \frac{A_t}{A_s} \right)^{1/3} \left( \frac{P_s}{P_t} \right)^{1/3} \frac{St_s}{St_t} + r \frac{k}{k_s} &= (1+r) \frac{A_t}{A_s} \\ \frac{k_t}{k_s} \left( \frac{A_t}{A_s} \right)^{1/3} &= \frac{(1+r)A_t/A_s - rk_t/k_s}{\frac{St_s}{St_t} \left( \frac{P_s}{P_t} \right)^{1/3} \left( \frac{f_t}{f_s} \right)^{1/3}} \\ \Rightarrow \frac{\frac{k_t}{k_s} \left( \frac{A_t}{A_s} \right)^{1/3}}{\left( \frac{P_s}{P_t} \right)^{1/3} [(1+r)A_t/A_s - rk_t/k_s]} &= \frac{\left( \frac{St_t}{St_s} \right)}{\left( \frac{f_t}{f_s} \right)^{1/3}} \end{aligned} \quad (20.10)$$

### Rough Surface Heat Exchanger tubes-10 Constant Pumping Power, Conductance

- Again do the same manipulations for the three cases. First consider  $P/P_s = k/k_s = 1$ . Start with equ<sup>n</sup> (20.5) and simplify:

$$\frac{k_t}{k_s} = 1 = \frac{A_t}{A_s} \frac{(1+r)}{g^* \left( \frac{St_s}{St_t} \right) + r} \quad (20.11)$$

$$\Rightarrow \frac{A_t}{A_s} = \frac{g^* St_s / St_t + r}{1+r} \quad (20.12)$$

- Start with equ<sup>n</sup> (20.8) to get:

$$\frac{P_t}{P_s} = 1 = \frac{f_t}{f_s} \frac{A_t}{A_s} \frac{1}{g^{*3}}$$

### Rough Surface heat Transfer: tubes-11 Constant Pumping Power, Conductance

- Use  $k/k_s = 1 = P/P_s = 1$  in equ<sup>n</sup> (20.10) and use equ<sup>n</sup> (20.13) to get

$$\begin{aligned} \frac{\left( \frac{A_t}{A_s} \right)^{1/3}}{\frac{1}{g^{*2}} \frac{A_t}{A_s} \left[ (1+r)g^{*2} - r \frac{f_t}{f_s} \frac{1}{g^*} \right]} &= \frac{St_t / St_s}{(f_t / f_s)^{1/3}} \\ \Rightarrow \frac{(A_s / A_t)^{2/3} g^{*2}}{(1+r)g^{*2} - r \frac{f_t}{f_s} \frac{1}{g^*}} &= \frac{St_t / St_s}{(f_t / f_s)^{1/3}} \\ \Rightarrow \frac{\left[ (f_t / f_s)^{2/3} 1 / g^{*2} \right] g^{*2}}{(1+r)g^{*2} - r \frac{f_t}{f_s} \frac{1}{g^*}} &= \frac{St_t / St_s}{(f_t / f_s)^{1/3}} \end{aligned} \quad (20.14)$$

## Rough Surface Heat Exchanger tubes-12

### Constant Pumping Power, Conductance

- Equ<sup>n</sup> (20.14) is simplified to yield the final expression:

$$\frac{f_t / St_t}{f_s / St_s} = g^{*2} (1+r) - \frac{r(f_t / f_s)}{g^*} \quad (20.15)$$

- Use equ<sup>n</sup> (20.15) to obtain g\*. Now use this in the A/As expression i.e. equ<sup>n</sup> (20.12), to verify whether it is less than unity or not.

## Rough Surface heat Transfer: tubes-13

### Constant Pumping Power, Area

- Next case P/Ps = 1, A/As = 1. Use equ<sup>n</sup> (20.13) to yield:

$$g^* = (f_t / f_s)^{1/3}$$

- Substitute in equ<sup>n</sup> (20.11) to yield

$$\frac{k_t}{k_s} = \frac{1+r}{(f_t / f_s)^{1/3} (St_s / St_t) + r} \quad (20.16)$$

- Note that this is the same as equ<sup>n</sup> (19.13) for r = 0 in equ<sup>n</sup> (20.16).

## Rough Surface heat Transfer: tubes-14

### Constant Area, Conductance

- Last case k/ks=1, A/As=1
- Use equ<sup>n</sup> (20.7)

$$1 = \frac{1+r}{(g^* St_s / St_t + r)} \Rightarrow g^* = St_t / St_s \quad (20.17)$$

- Use equ<sup>n</sup> (20.8) to get:

$$g^* = \frac{(f_t / f_s)^{1/3}}{(P_t / P_s)^{1/3}} \quad (20.18)$$

- Equate equ<sup>n</sup>s (20.17) and (20.18) to get:

$$\Rightarrow \frac{P_t}{P_s} = \frac{f_t / f_s}{(St_t / St_s)^3} \quad (20.19)$$

## Recap

### In this class:

- Methodologies for evaluation of the performance of heat transfer enhancement devices in heat exchanger tubes of tube in tube type
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