

Module 2 :

“Diffusive” heat and mass transfer

Lecture 12:

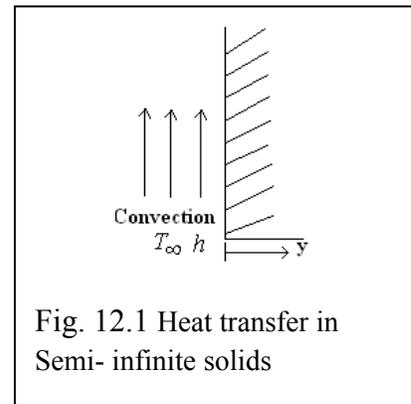
Heat Conduction in Semi-infinite Slab with Constant Flux density at the wall

Consider heat conduction in y -direction in a semi-infinite slab (bounded only by one face) initially at a temperature T_i , whose face suddenly at time equal to zero is raised to and maintained at T_1 . Assuming constant thermal diffusivity and with no heat generation, a differential equation in one space dimension and time is given by

$$\frac{\partial T}{\partial t} = \alpha \frac{\partial^2 T}{\partial y^2} \quad (12.1)$$

The initial condition (I.C) and boundary conditions (B.C) are

$$\text{I.C. } T(y,0) = T_i = \text{Constant} \quad (y > 0)$$



The condition of constant flux density, q_0 , can be achieved in a system where the object is exposed to a uniform source of energy. Such conditions can be observed in a fired heater, nuclear reactor, or solar collector, where the tube is exposed to a uniform source of radiation.

$$\text{B.C.1. } -k \left(\frac{\partial T}{\partial y} \right)_{y=0} = q_0 = \text{Constant} \quad (t > 0)$$

$$\text{B.C.2. } \lim_{y \rightarrow \infty} T(y,t) = T_i \quad (t > 0)$$

Setting $\theta = T - T_i$, so equation (12.1) becomes

$$\frac{\partial \theta}{\partial t} = \alpha \frac{\partial^2 \theta}{\partial y^2} \quad (12.2)$$

Accordingly I.C. and B.Cs will be

$$\text{I.C. } \theta(y,0) = 0$$

$$\text{B.C.1. } -k \left(\frac{\partial \theta}{\partial y} \right)_{y=0} = q_0$$

$$\text{B.C.2. } \theta \rightarrow 0 \text{ as } y \rightarrow \infty$$

Using Laplace transform to solve equation (12.2), we get

$$p \bar{\theta}(y,p) - \bar{\theta}(y,0) = \alpha \bar{\theta}_{yy}(y,p) \quad (12.3)$$

Using I.C. in equation (12.3), we get

$$p \bar{\theta} = \alpha \frac{\partial^2 \bar{\theta}}{\partial y^2} \quad (12.4)$$

The solution to equation (12.4) is

$$\bar{\theta} = C_1 \exp\left(y \sqrt{\frac{p}{\alpha}}\right) + C_2 \exp\left(-y \sqrt{\frac{p}{\alpha}}\right) \quad (12.5)$$

Applying B.C.2 in eqn. (12.5), we get

$$C_1 = 0$$

From B.C.1 and differentiation of eqn. (12.5) w.r.t y gives

$$-k C_2 \left(-\sqrt{\frac{p}{\alpha}} \right) = \frac{q_0}{p}$$

Evaluating C_2 and substituting in equation (12.5), we get

$$\bar{\theta} = \frac{q_0 \sqrt{\alpha}}{K_p \sqrt{p}} \exp\left(-y \sqrt{\frac{p}{\alpha}}\right) \quad (12.6)$$

From tables (refer H.S. Mickley, T.S. Sherwood, and C.E. Reed, Applied Mathematics in Chemical Engineering., McGraw-Hill, 1979)

$$\mathcal{F}^{-1}\left\{\frac{1}{\sqrt{p}} \exp\left(-y \sqrt{\frac{p}{\alpha}}\right)\right\} = \frac{1}{\sqrt{\pi t}} \exp\left(-\frac{y^2}{4\alpha t}\right) = F(y) \quad (12.7)$$

Division of the transform by 'p' corresponds to integration between 0 and t.

$$\mathcal{F}^{-1}\left\{\frac{1}{p} f(p)\right\} = \int_0^t F(z) dz \quad (12.8)$$

Thus using equation (12.6), (12.7) and (12.8) we can write

$$\theta = \mathcal{F}^{-1}\left\{\frac{q_0 \sqrt{\alpha}}{k} \frac{1}{p \sqrt{p}} \exp\left(-y \sqrt{\frac{p}{\alpha}}\right)\right\} = \frac{q_0 \sqrt{\alpha}}{k} \int_0^t \frac{1}{\sqrt{\pi z}} \exp\left(-\frac{y^2}{4\alpha z}\right) dz \quad (12.9)$$

Set $x = \frac{y}{\sqrt{4\alpha z}}$, equation (12.9) then becomes

$$\theta = \frac{q_0 y}{k \sqrt{\pi}} \int_{\frac{y}{\sqrt{4\alpha t}}}^{\infty} \frac{1}{x^2} \exp(-x^2) dx \quad (12.10)$$

On integration by parts, eqn. (12.11) gives

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$$\theta(y,t) = \frac{q_0}{k\sqrt{\pi}} \left[2\sqrt{\alpha t} \exp\left(-\frac{y^2}{4\alpha t}\right) - 2y \int_{\frac{y}{\sqrt{4\alpha t}}}^{\infty} e^{-y^2} dy \right] \quad (12.11)$$

or

$$\theta(y,t) = \frac{q_0}{k} \left[2\sqrt{\frac{\alpha t}{\pi}} \exp\left(-\frac{y^2}{4\alpha t}\right) - y \operatorname{erfc}\left(\frac{y}{\sqrt{4\alpha t}}\right) \right] \quad (12.12)$$

From equation (12.12) we can conclude that surface temperature increases as \sqrt{t} .

$$\theta(0,t) = \frac{2q_0\sqrt{\alpha}}{k\sqrt{\pi}} \sqrt{t} \quad (12.13)$$

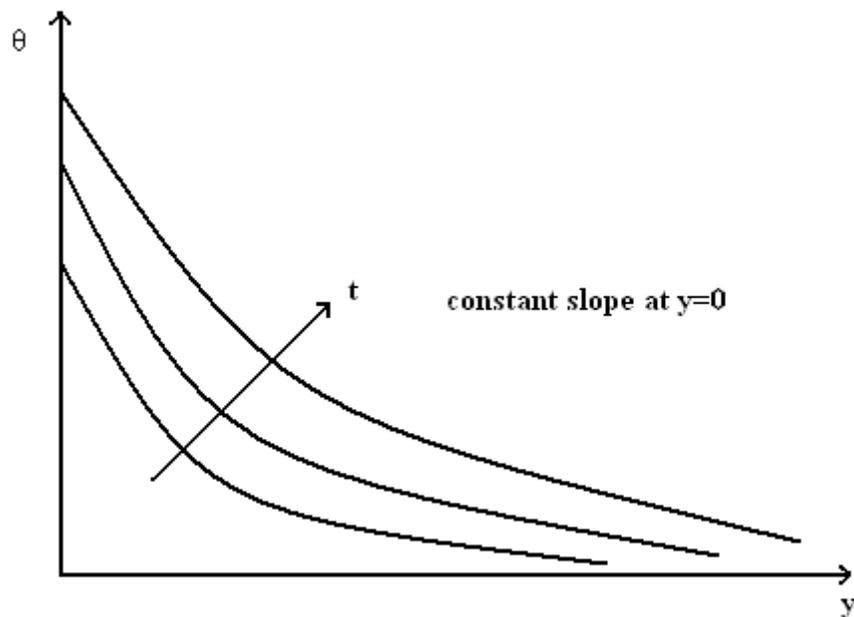


Fig. 12.1 Temperature varies with length at different time period