

Module 5: Reynolds Transport Theorem

Lecture 12: Conservation of mass and examples

 Conservation of mass

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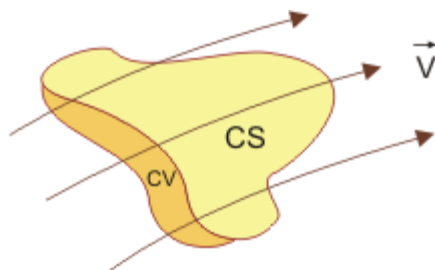
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Conservation of mass

$N = \text{property} = M$; Therefore, $\eta = 1$

Apply Reynold's Transport Theorem:



(Fig. 12a)

$$\frac{\partial}{\partial t} \iiint 1 \cdot \rho \, dV = \frac{D}{Dt} \iiint_{CV} 1 \cdot \rho \, dV - \oint_{CS} 1 \cdot (\rho \vec{V} \cdot d\vec{A})$$

(Particle-mass cannot be created or destroyed)

The 1st term of the right-hand-side is zero: particle-mass cannot be created or destroyed.

Therefore, $\frac{\partial}{\partial t} \iiint_{CV} \rho \, dV = - \oint_{CS} (\rho \vec{V} \cdot d\vec{A})$: conservation of mass equation

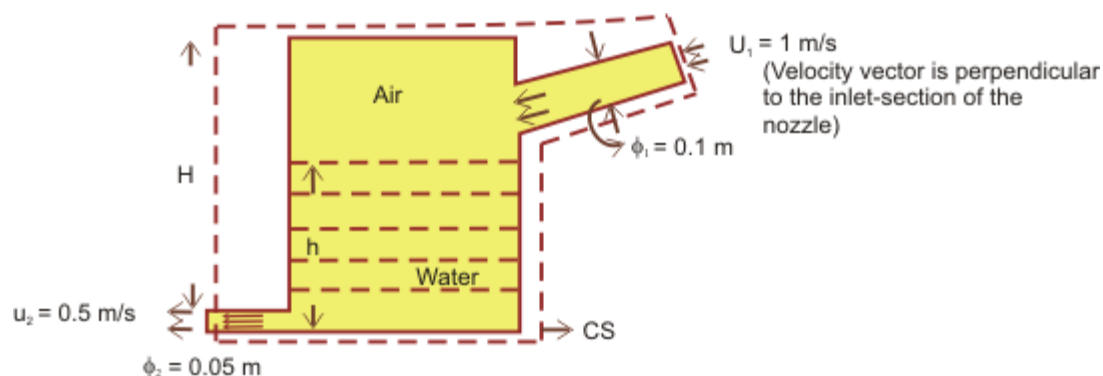
- Note that ρ of a fluid in a CV may change with time, for example, in a tank filled with air and water. If water is drained out, ρ of the mixture (air + water) will vary with time. Message: Be careful while evaluating the integral, whether ' ρ ' under evaluation refers to the density of a pure fluid or fluids-mixture.

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Example 1: Consider a closed tank partially filled with water. In such case air is trapped at the top. Tank is filled with water at the rate of 1m/s through a nozzle of 10 cm inside-diameter and drained from the bottom at the rate of 0.5m/s through a nozzle of 5 cm diameter. Determine the rate of change in the height of water. The diameter of the tank is 5 m.



(Fig. 12b)

Ans: Consider the **CV** drawn above. Note that **CV** is chosen in such a way that the **CS** is perpendicular to the inlet and outlet nozzles of the tank.

The LHS term of the Reynolds transport theorem or conservation of mass:

$$= \frac{\partial}{\partial t} \iiint_{CV} \rho \, dV = \frac{d}{dt} (\rho_w A_w h_w) + \frac{d}{dt} \rho_{air} A h_{air}$$

(where, $h_{air} = H - h_w$)

$$= \frac{d}{dt} (\rho_w A h_w) \left\{ \begin{array}{l} \text{2nd term} \\ \text{is zero because} \\ \text{total mass of air} \\ \text{does not change, as the air is trapped.} \end{array} \right.$$

$$\begin{aligned} \text{RHS} &\equiv - \iint_{CS} (\rho \vec{V} \cdot d\vec{A}) \\ &= -\rho_{water} (-V_1 A_1 + V_2 A_2) \end{aligned}$$

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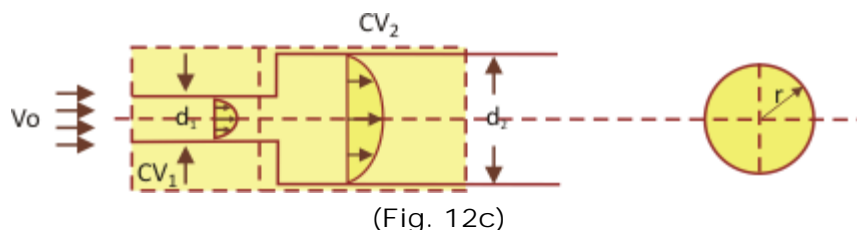
It is assumed that the water velocity is uniform over the inlet- and outlet ports. Also, note that the velocity vector of incoming water to the inlet of the tank is opposite to the area- vector.

Simplifying, $\rho_w A \frac{dh}{dt} = \rho_w (+V_1 A_1 - V_2 A_2)$

$$\frac{dh}{dt} = \frac{V_1 A_1 - V_2 A_2}{A} = \frac{1 \times (0.1)^2 - 0.5 \times (0.05)^2}{5^2}$$

$$= \frac{.01 - .00125}{25} = \frac{.00875}{25} = 0.00035 \text{ m/s}$$

Example 2: Consider the steady-state flow of water in a circular tube of variable area:



The velocity at the inlet to the tube is uniform at V_0 . The velocity profile in both sections of the tube is parabolic.

$$v(r) = V_{\max} \left(1 - \frac{r^2}{R^2} \right), \text{ where } R = d_1/2 \text{ or } d_2/2$$

Apply the conservation of mass equation to calculate maximum velocity in the tube (both sections) in terms of known quantities.

Consider CV_1 :

$$\frac{\partial}{\partial t} \iiint \rho \, dV = - \iint_{CS_1} (\rho \vec{V} \cdot d\vec{A})$$

(1st term is zero for steady-state condition)

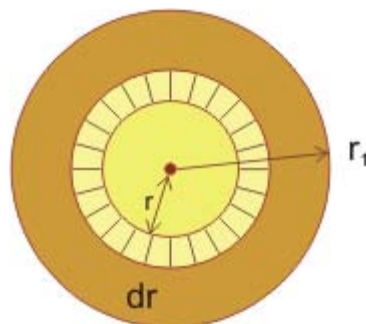
Therefore, $\iint_{CS} \vec{V} \cdot d\vec{A} = 0$

$$: V_0 A_1 = \int_0^{r_1} v(r) 2\pi r dr, \text{ where } \begin{cases} A_1 = \pi/4 d_1^2 \\ r_1 = d_1/2 \end{cases}$$

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The RHS of the above equation is the integral (over the entire cross-section) of the differential volumetric flow rate:



(Fig. 12d)

$$V_0 \frac{\pi}{4} d_1^2 = \int_0^{r_1} v_{\max} \left(1 - \frac{r^2}{r_1^2}\right) 2\pi r dr \quad \left\{ \begin{array}{l} \text{differential volumetric} \\ \text{flow rate, } dq \text{ is} \\ v(r) 2\pi r dr \end{array} \right.$$

$$V_0 \pi r_1^2 = 2\pi v_{\max} \int_0^{r_1} \left(1 - r^2/r_1^2\right) r dr = 2\pi v_{\max} \left(\frac{r^2}{2} - \frac{r^4}{4r_1^2} \right) \Big|_0^{r_1}$$

$$= \pi v_{\max} r_1^2 / 2$$

Or $\boxed{v_{\max} = 2 V_0}$ Ans.

Apply the conservation law again over larger CV_2 to show that,

$$V_0 \pi r_1^2 = \pi v_{\max} \frac{r_2^2}{2}$$

$$\boxed{v_{\max} = 2 \left(\frac{r_1}{r_2} \right)^2 V_0} \text{ Ans.}$$

Further, v_{\max} (for the 2nd section) = v_{\max} (for the 1st section) $\times \left(\frac{r_1}{r_2} \right)^2$

or, $(V_{\max} A)_1 = (V_{\max} A)_2$

Re-visit, $\iint_{CS} \vec{V} \cdot d\vec{A} = 0 \Rightarrow \iint_{CS} dq = 0$

or, $Q_1 = Q_2$ (volumetric flow rate)

or, $(\bar{V} A)_1 = (\bar{V} A)_2$, where \bar{V} = average velocity in the section

Compare to $(V_{\max} A)_1 = (V_{\max} A)_2$ to show that $V_{\max} = 2\bar{V}$.