

Module 5: Premixed Flame

Lecture 27: Flame Stabilization

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Turbulent Flame Regimes

Turbulent Flame Regimes

Reynolds number for turbulent flame:

$$Re_t = \frac{V'_{rms} l_0}{\nu}$$

Chemical reaction time:

$$\tau_{ch} = \frac{\delta_L}{S_L}$$

Chemical reaction time:

$$\tau_t = \frac{l_0}{V'_{rms}}$$

Damkohler number

$$Da = \frac{t_m}{t_{ch}} = \frac{l_0/V'_{rms}}{\delta_L/S_L}$$

If $Da \gg 1$, fast chemistry regimeIf $Da \ll 1$, fast mixing regime
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The Borghi Diagram

Borghi Diagram

- The plot of Da against Re_1 on a log-log scale
- Depicts various regimes of turbulent flames

Weak turbulent flame

- Upper region of the Borghi diagram

Wrinkled laminar flame

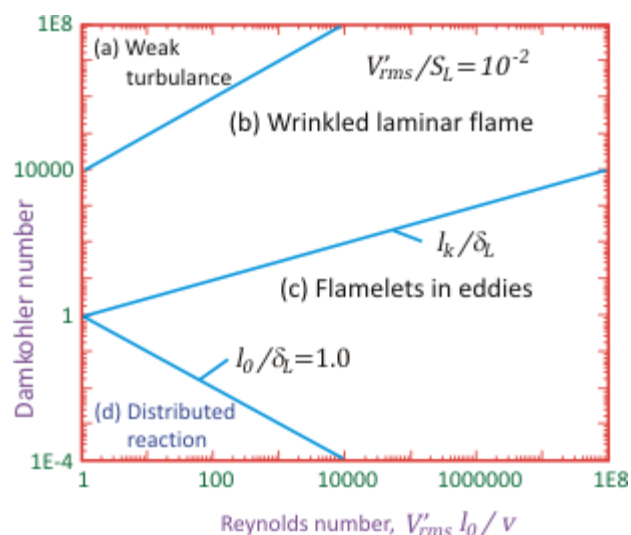
- Region between $V'_{rms}/S_L = 10^{-2}$ and l_k/δ_L
- Chemical reaction takes place in a thin zone

Flamelets in eddies

- Region between upper bold line $l_k/\delta_L = 1$ and $l_0/\delta_L = 1$

Distributed reaction regime

- Region below $l_0/\delta_L = 1$
- Reaction sheets are distributed in the turbulent flame surface ($Da < 1$)
- This type of combustion can be established in a well stirred reactor.



(Figure 27.1)

Turbulent Burning Velocity

Turbulent burning Velocity
(S_T)

- Depends on characteristics of fluid flow
- Velocity at which unburnt mixture enters the flame zone
- Difficult to measure velocity of unburnt gas near the turbulent flame

How to measure (S_T) ?

From the reactant flow rate

$$S_T = \frac{\dot{m}}{A\rho_u}$$

Turbulent Burning Velocity

$$\frac{S_T}{S_L} = \left(\frac{\alpha_T}{\alpha_L}\right)^{0.5}$$

\dot{m} is the reactant flow rate

\bar{A} is the time average flame surface area

ρ_u is the density of unburnt gas

Weak Turbulent
Flame

- Extension of laminar flame (low turbulence level)
- Smooth flame
- Turbulence scale \approx Laminar flame thickness
- $S_T > S_L$ Why? increase in
thermal diffusion

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Wrinkled Laminar Flame

- Flamelets in flame surface propagate at laminar burning velocity
- Turbulence only causes wrinkling of flame



(Figure 27.2)

Turbulent burning velocity is given by,

$$m = \rho_u \bar{A} S_T = \rho_u A_{F1} S_L \Rightarrow \frac{S_T}{S_L} = \frac{A_{F1}}{\bar{A}}$$

According to Damkohler, for constant laminar burning velocity

$$\frac{A_{F1}}{A} = \frac{V_u}{S_L}$$

Similarly for turbulent flame,

$$\frac{A_w}{A} = \frac{V'_{rms}}{S_L}$$

$$\frac{S_T}{S_L} = \frac{\bar{A} + A_w}{\bar{A}} = \left(1 + \frac{V'_{rms}}{S_L} \right)$$

According to Klimov,

$$\frac{S_T}{S_L} = 3.5 \left(\frac{V'_{rms}}{S_L} \right)^{0.7}$$

According to Calvin and William,

$$\frac{S_T}{S_L} = \left[0.5 \left\{ 1 + \left(1 + \frac{8CV'^2_{rms}}{S_L^2} \right) \right\}^{0.5} \right]^{1/2}$$

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Distributed Reaction

- For high intensities of wrinkling, distinct regime with small pockets of reactants are formed.
- In Borghi's diagram, this lies in the regime where integral length scale and Damkohler number are less than unity.
- Quite difficult to occur in practical devices.
- In laboratory, such situation can be created by using stirred reactor.
- Chemical reactions are not completed in reaction zone; rather occur in post-flame region.
- This regime needs more understanding.



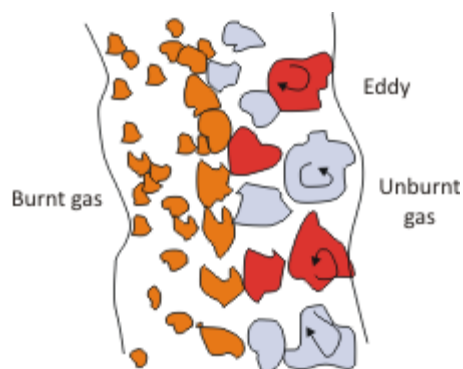
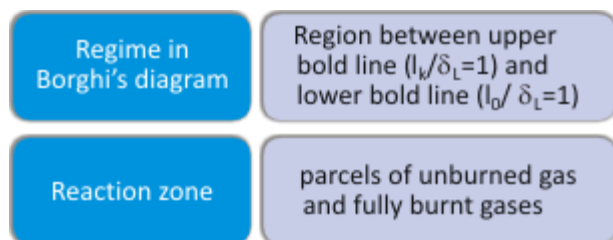
(Figure 27.3)

Turbulent burning velocity is given by,

$$S_T = 6.4 V'_{rms} \left(\frac{\bar{V}}{V'_{rms}} \right)^{3/4}$$

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Flamelet in Eddies



(Figure 27.4)

Fuel mass burning rate,

$$\dot{m}_F''' = -\rho C_F Y'_{F,rms} \varepsilon_o / ke_t$$

Typically, $C_F = 1$; $Y'_{F,rms}$ is root mean square of fluctuating fuel mass fraction, ke_t is the turbulent kinetic energy per unit.

$$\dot{m}_F''' = -\rho C_F Y'_{F,rms} V_{rms} / l_o$$

Examples:

- SI Engines
- Premixed burner
- High velocity burner

References

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2. Stephen R. Turns, An Introduction to Combustion, McGraw Hill Publication, Singapore, 1996.
3. Irvin Glassman, Combustion, Academic Press, New York, 1977.