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Courses » Upstream LNG Technology

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Unit 7 - Week 6

Course outline

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Week 6

- Lecture 35 : Estimation of water content in natural gas
- Lecture 36 : Multistage single component equilibrium separation
- Lecture 37 : Tutorial on vapour liquid separation
- Lecture 38 : Tutorial on ideal binary distillation
- Lecture 39 : Tutorial on equilibrium gas-solid separation
- Lecture 40 : Tutorial on membrane gas separation

Week 6 Assignment 6

The due date for submitting this assignment has passed. **Due on 2018-09-12, 23:59 IST.**
As per our records you have not submitted this assignment.

1) Which among the following is not a direct contact separation process **1 point**

- a) Distillation
- b) Membrane separation
- c) Absorption
- d) Adsorption

No, the answer is incorrect.

Score: 0

Accepted Answers:

b) Membrane separation

2) Extraction is used for the separation of **1 point**

- a) Liquid – Liquid system
- b) Liquid – Vapor system
- c) Liquid – Solid system
- d) Gas – Solid system

No, the answer is incorrect.

Score: 0

Accepted Answers:

a) Liquid – Liquid system

3) Leaching is used for the separation of **1 point**

- a) Liquid – Liquid system
- b) Liquid – Vapor system
- c) Liquid – Solid system
- d) Gas – Solid system

No, the answer is incorrect.

Score: 0

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c) Liquid – Solid system

d) Gas – Solid system

No, the answer is incorrect.

Score: 0

Accepted Answers:

b) *Liquid – Vapor system*

5)

1 point

The relative volatility of A in a mixture with B is $\alpha_{AB} = 2.5$. The equilibrium vaporization ratio of B is $K_B = 0.7$. The value of α_{BA} ?

Given:

$$\alpha_{AB} = 2.5$$

$$K_B = 0.7$$

To Find:

$$\alpha_{BA}$$

a) 0.4

b) 0.5

c) 0.7

d) 0.8

No, the answer is incorrect.

Score: 0

Accepted Answers:

a) *0.4*

6) The relative volatility of A in a mixture with B is $\alpha_{AB} = 2.5$. The mole fraction of B in the first **1 point** droplet of liquid condensed from an equimolar saturated vapor mixture of A and B is about

Given:

$$\alpha_{AB} = 1.5$$

Equimolar saturated vapor mixture i.e.,

$$y_A = y_B = 0.5$$

To Find:

$$x_B$$

a) 0.45

b) 0.51

c) 0.71

d) 0.80

No, the answer is incorrect.

Score: 0

Accepted Answers:

c) *0.71*

7) Consider a mixture of 30 mole% A, 30% B and 40% C. The solution is approximately ideal. The **1 point** following relative volatility values are known at 1 atm pressure: $\alpha_{AB} = 1.4, \alpha_{CB} = 1.2$. The value of α_{CA} is

Given:

$$\alpha_{AB} = 1.4$$

$$\alpha_{CB} = 1.2$$

To Find:

$$\alpha_{CA}$$

- a) 0.21
- b) 0.57
- c) 0.41
- d) 0.86

No, the answer is incorrect.

Score: 0

Accepted Answers:

d) 0.86

8) A ternary solution of A (30 mole%), B (40 mole%) and C may be considered to be ideal. The equilibrium vaporization ratios are $K_1 = 2.25$, $K_2 = 1.02$ and $K_3 = 0.6$ at 1 atm total pressure. The solution is: **1 point**

Given:

$$K_1 = 2.25$$

$$K_2 = 1.02$$

$$K_3 = 0.6$$

$$x_1 = 0.3$$

$$x_2 = 0.4$$

$$x_3 = 0.3$$

- a) Below the bubble point
- b) Saturated liquid
- c) Above the bubble point
- d) Saturated vapor

No, the answer is incorrect.

Score: 0

Accepted Answers:

c) Above the bubble point

9) Water content of natural gas drops with increase in **1 point**

- a) Temperature
- b) Pressure
- c) Amount of liquefied acid gases
- d) Molecular weight

No, the answer is incorrect.

Score: 0

Accepted Answers:

a) Temperature

d) Molecular weight

10) Which of the following analytical method is NOT used for water estimation in sour natural gas **1 point**

- a) Zhu et al. method
- b) Maddox's component contribution model
- c) Robinson's H₂S model
- d) Wang et al. method

No, the answer is incorrect.

Score: 0

Accepted Answers:a) *Zhu et al. method*11) 500 ppmv CO₂ in air at 25°C and 1 atm is equivalent to**1 point**

- a) 1121.0 mg/m³
- b) 599.7 mg/m³
- c) 500.0 mg/m³
- d) 899.7 mg/m³

No, the answer is incorrect.**Score: 0****Accepted Answers:**d) *899.7 mg/m³*

12) Dehydration reduces:

1 point

- a) The chances of gas hydrate formation in natural gas.
- b) The corrosion in natural gas pipelines.
- c) The heating value of the natural gas.
- d) The cost of separation of water.

No, the answer is incorrect.**Score: 0****Accepted Answers:**a) *The chances of gas hydrate formation in natural gas.*b) *The corrosion in natural gas pipelines.*c) *The heating value of the natural gas.*

13)

1 point

12 m³ of oxygen is to be separated by adsorption using silica gel at 30 kPa and 90.1 K. The saturation pressure of O₂ at 90.1 K is 100.4 kPa. The mass of silica gel required for this purpose is about (Hint: Isotherm using the parameters given in Table 1.)

Adsorbent	Gas	Temperature		v_m		θ_s	
		K	°R	dm ³ /kg	ft ³ /lb _m	K	°R
Unpromoted Fe catalyst	N ₂	90.1	162.2	0.268	0.0043	389.6	701.3
Fe-Al ₂ O ₃ catalyst	N ₂	90.1	162.2	2.091	0.0335	389.6	701.3
Cr ₂ O ₃ gel	N ₂	90.1	163.2	50.50	0.809	371.6	668.8
Silica gel	N ₂	90.1	162.2	127.0	2.034	399.8	719.6
Silica gel	N ₂	90.1	162.2	135.2	2.166	362.2	651.9
Silica gel	A	90.1	162.2	122.0	1.955	299.7	539.4
Silica gel	O ₂	90.1	162.2	132.0	2.115	295.5	531.9
Silica gel	CO	90.1	162.2	132.0	2.115	490.6	883.1
Silica gel	CO ₂	195	351	102.4	1.640	672.5	1210.5
Charcoal	H ₂ O	283	509	185.4	2.97	-327.7	-589.8
Charcoal	H ₂ O	258	464	185.4	2.97	0	0
Charcoal	N ₂	77.3	139.2	181.5	2.908	300.2	540.4
Charcoal	N ₂	90.1	162.2	173.0	2.772	331.6	596.8
Charcoal	A	77.3	139.2	215.6	3.454	341.1	613.9
Charcoal	A	90.1	162.2	215.6	3.454	376.8	678.3
Charcoal	O ₂	90.1	162.2	234.7	3.760	192.5	346.5
Charcoal	CO	90.1	162.2	179.7	2.878	246.9	444.4

- a) 61.3 kg
- b) 109.5 kg
- c) 21.4 kg
- d) 156.0 kg

No, the answer is incorrect.

Score: 0

Accepted Answers:

a) 61.3 kg

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