#### ME-662 CONVECTIVE HEAT AND MASS TRANSFER

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LECTURE-2 FLOW CLASSIFICATIONS

### **LECTURE-2 FLOW CLASSIFICATIONS**

#### Purpose

Plow Types and Present Selection

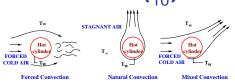
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## Purpose - L2( $\frac{1}{10}$ )

- In Convective Heat & Mass Transfer, we are concerned with Bulk Fluid Motion.
- As such, everything that affects Bulk Flow, influences 'h' and 'g'
- All flows are governed by 3D, time-dependent Partial Differnetial Equations (PDEs) of Mass, Momentum and Energy transfer
- Not all flows can be elegantly treated by Analytical Methods. Hence, Numerical Methods become necessary
- Complete equations under all types of boundary conditions and complexities of flow domains can only be solved by Computational Fluid Dynamics techniques.
- The scope of the subject is very vast. Hence, one must deal with Classes of Flows

## Forced and Free Convection - $L2(\frac{2}{10})$

- If the fluid motion is caused by external means ( pump, blower etc ) - Forced Convection
- If the fluid motion is induced by Density differences arising from Temperature differences, - Free or Natural Convection
  - If the two motions are comparable - Mixed Convection

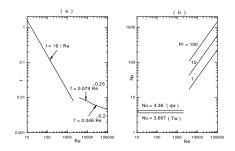


- $Nu_m = C \operatorname{Re}_D^m \operatorname{Pr}^m$  (Forced  $Gr/\operatorname{Re}^2 << 1$ )
- 2  $Nu_m = C Gr_D^m Pr^m$  (Free  $Gr/Re^2 >> 1$ )
- $Nu_m = C (Gr/Re^2)_D Pr^m$  (Mixed  $Gr/Re^2 \simeq 1$ )
  - Grshof number Gr is ratio of Buoyancy and Viscous Forces

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## Laminar and Turbulent Flows - L2( $\frac{3}{10}$ )

- Reynolds number is the ratio of Inertia and Viscous Forces
- If Re < Re<sub>cr</sub> Laminar
- If Re > Re<sub>cr</sub> Turbulent
- If Re  $\simeq Re_{cr}$  Transition
- For Ducted flows,  $Re_{cr} \simeq 2200$
- Critical Reynolds or Grashof numbers are estimated for all types of flows



## Incompr and Compr Flows - L2( $\frac{4}{10}$ )

#### Incompressible Flows

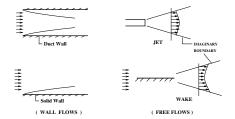
- Routinely occur in Liquids
- In Gases , Incompressible Flows occur when Mach number Ma =  $V/{\it V_{sound}} < 0.3$
- Solution Density is constant or, function of Temperature  $\rho(T)$  only

#### Ocompressible Flows

- Occur in Gases
- Ususally, *Ma* > 0.3
- Solution Density is function of Pressure and Temperature  $\rho(p, T)$

## Wall and Free Flows - L2( $\frac{5}{10}$ )

- We are interested in determining 'h' or 'g' at the interface between Solid-Liquid/Gas or between Liquid-Gas
- Flows with such interfaces are termed as
  Wall Flows . ( eg. Internal Duct Flow, External Flow over Tube, Wind flow over a Lake )
- Our interest is in Wall Flows only



In Free Flows such as Jets or Wakes, there are no interfaces. (eg. Discharge of hot water into a Water Body, Flow behind a Ship) Hence, not of interest.

# Boundary Layer and Recirculating Flows - L2( $\frac{6}{10}$ )

- Long and Thin Flows are called Boundary Layer Flows.
- Boundary layer flows are predominantly unidirectional One-Way Influence
- Flows are governed by Parabolic Equations



TWO-WAY INFLUENCE

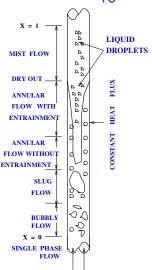


Recirculating Flow over a Surface Mounted Rib

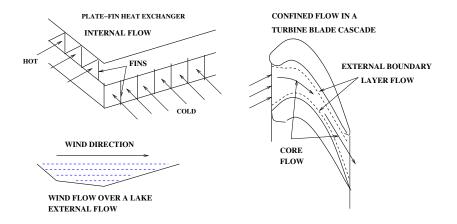
- In Recirculating Flows, there is no predominant flow direction - Two-Way Influence
- Flows are governed by Elliptic Equations

## Single and Two Phase Flows - $L2(\frac{7}{10})$

- Two Phase Flows are encountered in Evaporators, Cyclone Separators, Boiling Water Reactors, Fluidised Bed Dryers or PF Combustors etc.
- Involve Simultaneous H & M Transfer with or without Phase Change
- Complex Physics and Mathematics

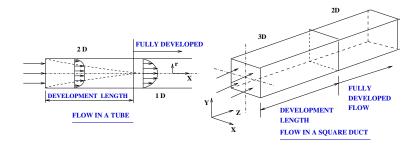


## Internal and External Flows - L2( $\frac{8}{10}$ )



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## 1D-2D-3D Flows - L2(<sup>9</sup>/<sub>10</sub>)



Flow-Dimensionality is determined by number of Independent variables (or, cooridinates) on which Flow Variables such as pressure, velocity, temperature etc depend.

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## Scope of Present Lectures - $L2(\frac{10}{10})$

- Forced and Free Convection
- Laminar and Turbulent Flows
- Incompressible and Compressible Flows
- Boundary Layer and Recirculating Flows
- Wall and Free Flows
- Single and Two Phase Flows
- 1D-2D -3D Flows

Flow Situations marked in Blue will be covered in this Course.